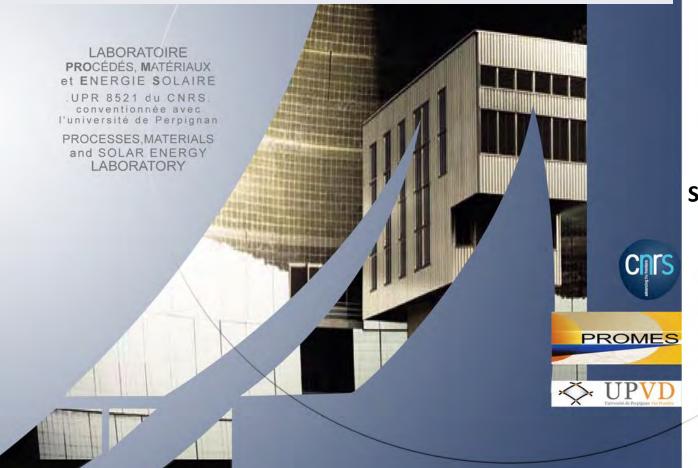
MW-scale prototype of the fluidized particles-in-tube solar receiver.

Implementation, Design and Control of the setup at Themis tower.









SolarPACES conference

September 30, 2020 On-line event

A. Le Gal, B. Grange, G. Flamant

PROMES-CNRS







- Presentation of the Next-CSP project
- Technology concept
- MW-scale design
- Human Machine Interface
- Loop control







Next-CSP project



10 partners, one objective :

Improving the reliability and performance of concentrated solar power plants through the development and integration of a new technology based on the use of fluidized particles in tube as heat transfer fluid and storage medium. (TRL 5)









Next-CSP project



Themis solar facility - Targassonne



1MW Solar furnace - Odeillo





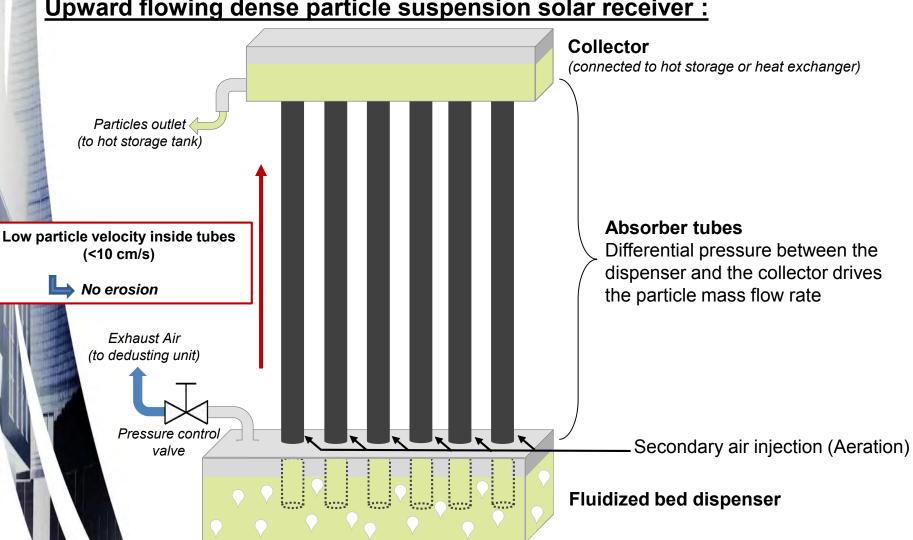




Technology concept



Upward flowing dense particle suspension solar receiver :



Fluidized bed air feeding



Technology concept

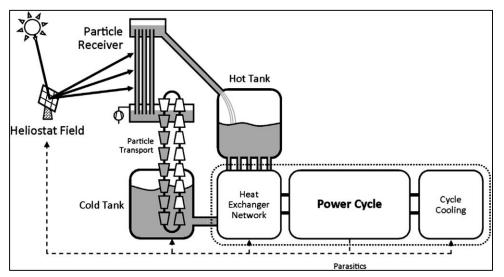


Advantages of this concept:

- Possibility to reach higher temperature than conventional heat transfer fluids (temperature up to 750°C could considerably improve the thermodynamic cycle efficiency) → Combined cycle, supercritical CO₂ cycle
- Direct storage of heat through the heat transfer fluid
- No freezing problems
- Good scalability of the concept (multi-tubular solar receiver)

Drawback:

Limited heat exchange between particles and the receiver wall surface



Generic layout of the dense particle suspension power plant. [1]



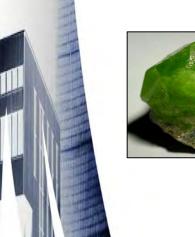


Technology concept



Olivine particles:

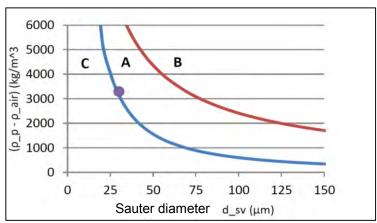
Particle	Composition	Mean diameter (d ₅₀) - μm	Sauter diameter (d ₃₂) - μm	Density - kg/m³	Bulk conductivity at 800°C – W/mK
Olivine	MgO 49.5%, SiO ₂ 42%, Fe ₂ O ₃ 7.5%	59	30	3300	0.56



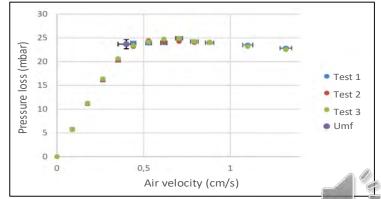




- Selected Olivine particles are part of the group A in the Geldart classification.
- The minimum air velocity to fluidized the particles is U_{mf}= 0.40 cm/s



Geldart classification of the selected olivine particles



Determination of the olivine particles minimum fluidization velocity (U_{mf}) .

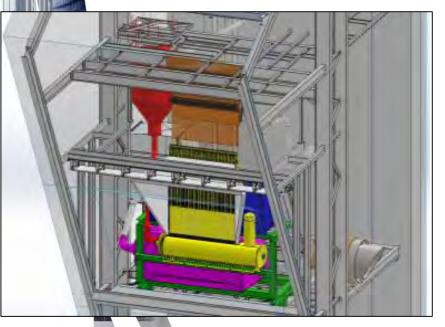
REF: Kang Q. et al., Particles in a circulation loop for solar energy capture and storage, Particuology, 43:149-156, 2019

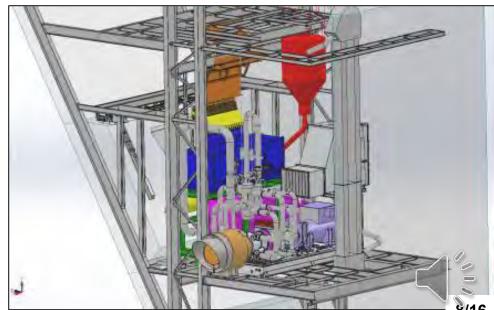


MW-scale design



- A 3 MW_{th} solar receiver has been assembled at the top of the THEMIS solar tower to demonstrate this technology in a relevant environment.
- A storage system composed of a cold and a hot tank
- A multi-stage heat exchanger
- An innovative 1.2 MW_{el} hybrid turbine (*OPRA turbine Solar/gasoil*)
- A 10 meters high bucket elevator





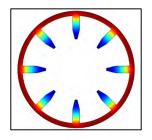


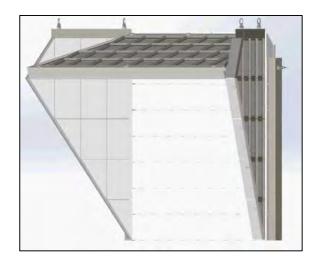
The solar receiver



- A dispenser to fluidize particles With homogeneous air injection through drilled tubes, (low air velocity $U_{mf} = 0.4$ cm/s \rightarrow low air flow)
- 40 tubes with 8 fins to favour heat transfer (316 SS, 3-meters high)
- A refractive cavity to improve the receiver's thermal efficiency







- Fully equipped with 100 thermocouples (front/back surface, inside tubes & dispenser)
 - Differential pressure sensors to measure the pressure drop inside tubes, inside dispenser.



Heat storage



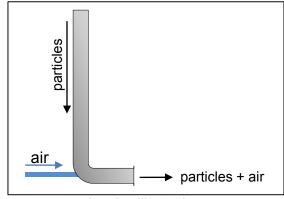
A cold storage tank



Level sensors to check the filling of the tank

Particle filling through a 10 meters high bucket elevator

a L-valve to empty the cold tank



L-valve illustration

A hot storage insulated tank

Low airflow to fluidize particle inside tank to allow particle transfer to heat exchanger (via a L-valve)

Half an hour of storage capacity (~20 tons of particles)



Top view of the hot storage with receiver's tubes connexion 0/16

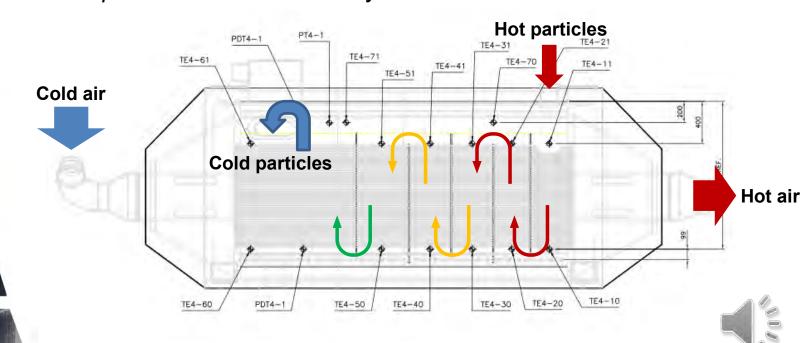


Heat exchanger



Fluidized particle/Air heat exchanger

- Hot particles from hot storage tank
- Compressed air from turbine compressor
- 6 stages
- 1200 tubes
- At the oultet particles are recovered by the bucket elevator





Hybrid turbine



- 1.2 MWel hybrid turbine
- Solar/Gasoil (first of it kind) OPRA development
- Connected to the heat exchanger with a fully automated control of the combusted gasoil flow in function of air temperature at the outlet of the heat exchanger





Control command



- Control/Command by using a Labview HMI
- What to control:
 - T_{max} receiver

 - $T_{\text{particles}}$ P_{sky} dispenser
 - $\Delta P_{dispenser}^{\text{f}}, \, \Delta P_{hot \, storage}, \, \Delta P_{heat \, exchanger}$
 - ΔP_{tubes}
- What to operate:
 - Fluidization air flowrates
 - Dispenser freeboard pressure
 - L-valves air injection







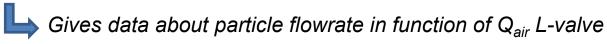


Loop control



How to measure particle flowrate?

- -1- Calibrate L-valves particle flowrates
 - for several Q_{air} L-valve, plot $\triangle P_{dispenser} = f(t)$ (follow the filling of the dispenser in function of time) (the height of the fluidized bed is directly correlated to the pressure drop of the bed)



- -2- Establish a correlation between the particle flowrate and P_{sky} dispenser
 - Test plan of particles circulation through the receiver's tubes for different dispenser freeboard pressure (P_{sky}) .
 - Set Q_{air} L-valve to keep $\Delta P_{dispenser}$ constant (No emptying of the fluidized bed)
 - Plot $\dot{m}_{particle} = f(P_{sky})$

-3- Establish a correlation between Q_{air} L-valves and P_{sky} dispenser to maintain the dispenser filling stable

Program the control (enslavement) of Q_{air} L-valve in function of P_{sky}







Acknowledgements









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Questions?



